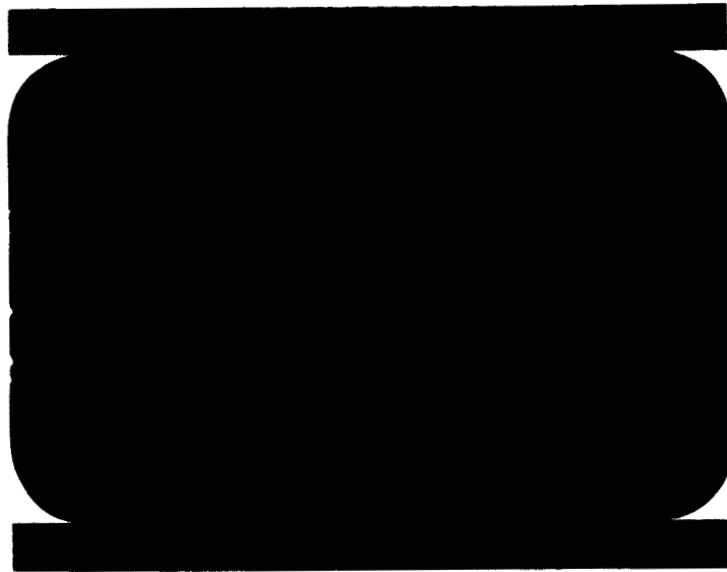


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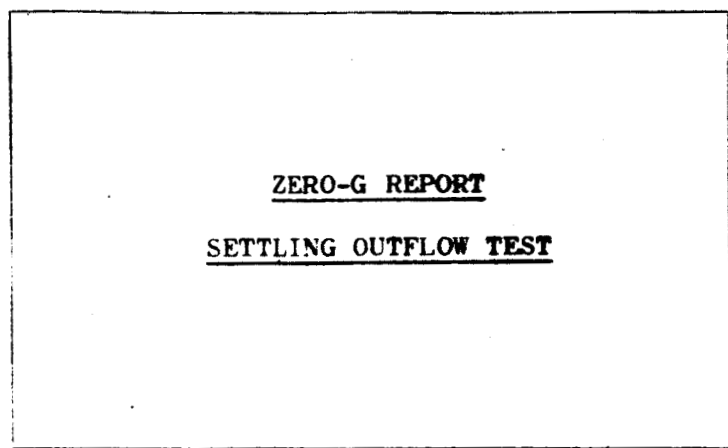
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GENERAL DYNAMICS  
ASTRONAUTICS

ff 653 July 65

# CONVAIR | ASTRONAUTICS

CONVAIR DIVISION OF GENERAL DYNAMICS CORPORATION



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## REVISIONS

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S U M M A R Y

Prior to Centaur engine restart the settling rockets will cause sloshing or turbulence of the fuel which may effect the chill down outflow. Slosh tests were conducted in a modified 3/20th-scale Centaur fuel tank to study this effect. A fixed time (measured from the start of settling) of between 1.4 and 2.2 seconds was required before clear flow (i.e., no entrained gas bubbles) was obtained. The time at which flow started did not influence the clear up time.

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SETTLING OUTFLOW TEST1.0 INTRODUCTION AND OBJECTIVE:

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The Centaur liquid-hydrogen fuel will, during the coast phase, be distributed around in its tank. When the settling rockets fire, the forward part of the liquid will move aft, causing turbulence and sloshing when it reaches the intermediate bulkhead or the LH<sub>2</sub> in that vicinity. The sloshing may appreciably affect the fuel-tank outflow during engine chill down. The tests described in this report were instituted to determine how much and in what manner the sloshing affects the outflow.

A scale model of the Centaur fuel tank was used to conduct the tests. The top of the tank was modified to allow a portion of the fuel to fall toward the aft bulkhead under a one-g acceleration. The results may be converted by Froude Number scaling to predict full size Centaur sloshing phenomena in any finite acceleration field.

Stoddard solvent was used to simulate liquid hydrogen because it wets the tank walls. Tests were conducted with no sloshing (i.e., no liquid settling) to establish a reference for the slosh effects.

## 2.0 TEST APPARATUS:

The test apparatus, Figure 1, consisted of a modified 3/20-scale model of the Centaur fuel tank. Total tank volume was about 4.5 ft<sup>3</sup>. Part of the "fuel" was held in the upper part of the tank by the dump valve which was spring loaded and manually actuated. See Figure 2. A fuel flow valve was placed below the outlet elbow. See Figure 3. Micro-switches, located on the fuel flow valve and on the dump valve actuator, indicated the valve openings by lights placed above the outlet elbow. A motion picture camera was used to monitor the liquid outflow and to observe the lights. The flow rate was controlled by varying the tank pressure. (Maximum operating pressure was 15 psig).

### 3.0 TEST PROCEDURE:

#### 3.1 Pre-Test Calibrations:

The volume flow rate as a function of driving pressure (i.e., tank pressure plus liquid head) was determined with a stop watch and a graduated container (c.f. Figure 4). Motion pictures were used to determine the time required for the liquid to fall to the intermediate bulkhead. The liquid and the release-time light were viewed by the camera. By counting the film frames between release and liquid contact with the aft bulkhead area, and knowing the film speed, the time for the liquid to fall was determined. The average time for the liquid to reach the bulkhead area was .32 seconds.

#### 3.2 Outflow Tests - No Settling:

Tests were first conducted with a still pool of liquid to establish a comparison for the effects of sloshing and bubble entrainment on the out flow. The time at which terminal pull through started was measured for various flow rates and liquid volumes (amount of liquid initially in the tank).

#### 3.3 Slosh Outflow Test:

To determine the effect of settling, the following information was recorded on motion picture film:

- 1) The time of liquid release.
- 2) The time of flow valve opening.
- 3) The time of flow valve closing.
- 4) The condition of flow (i.e., pull through vs. clear flow).
- 5) The % vapor present when the flow valve was closed.

#### 4.0 RESULTS AND DISCUSSION:

##### 4.1 Outflow Test - No Settling:

The detailed results of outflow from a still pool are given in Table I. The "Volume Remaining at Start of Pull Through" is the fill volume less the product of the flow rate and the time before terminal pull through. The "Liquid Height" above the peripheral joint was calculated from the volume remaining and a knowledge of the bulkhead shape. The top of the outlet elbow was about 3 inches above the peripheral joint (cf Figure 3). Hence the "Pull Down Distance" is the "Liquid Height" minus three inches. The outflow velocity was always high enough that any gas pulled into the elbow inlet was immediately carried through the smaller elbow outlet. Hence the top of the elbow (rather than the outlet tube itself) was taken as the reference point for the pull down distance. This distance was between one and three inches.

##### 4.2 The Slosh Outflow Tests:

4.2.1 Settling during the outflow tests caused vapor pull-through as the flow valve was opened. The quantity of vapor entrained decreased gradually as the flow continued. There was no clean cut off to the pull through, but the time at which the gas quantity was reduced to below 2% could be roughly estimated. This initial pull-through was still present for valve opening delays (time of liquid contact to time of flow start) near one second. See Tabel II and Figure 5. Note that between 1.4 and 2.2 seconds after the start of flow the initial pull-through cleared up (excepting the odd 27 - 0 % case). The time for start of clear flow does not seem to be a function of the time that the flow valve was opened or of the flow rate or of the "fuel" volume. There seems to be simply a fixed time required for the settling disturbance to die down enough that no gas is pulled through.



#### 4.0 RESULTS AND DISCUSSION: (Continued)

- 4.2.2 Note that in three of the  $3\frac{1}{4}$  /  $3\frac{1}{4}$  volume tests the flow valve was left open until after the terminal pull-through started. Tests with no settling showed that for this volume and flow rate that terminal pull occurred about 2.3 seconds after opening the flow valve. In these three cases the flow times were 2.16, 2.02, and 2.00 seconds or essentially the same as the no-settling tests. This result indicates that only a small percentage of gas is entrained during the initial pull-through, but the fraction of gas appeared to be large in the movies. No measure of this fraction was made during the tests nor could a reasonable estimate be made from the movies.

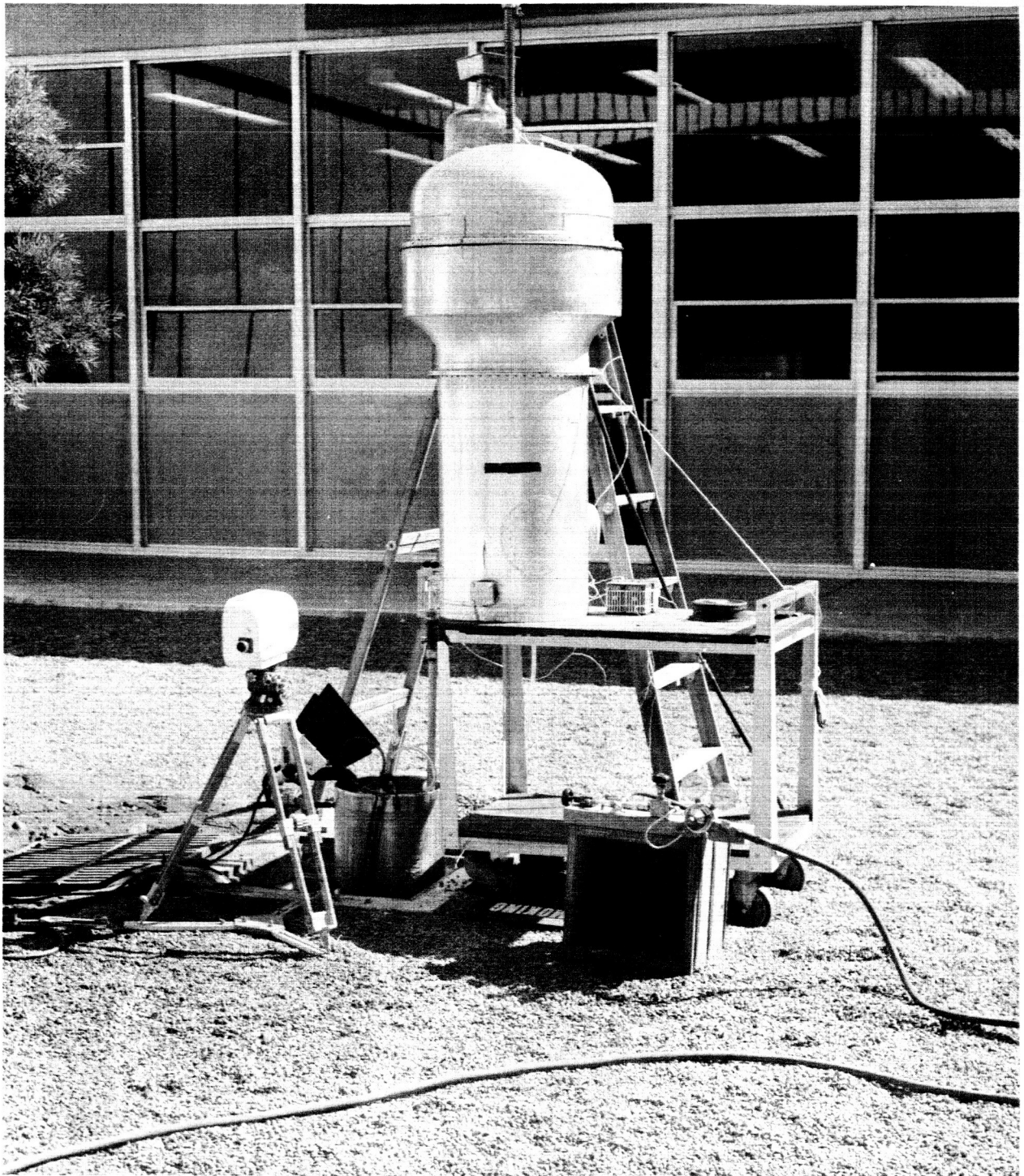
TABLE I ----- OUTFLOW TEST - NO SETTLING

% Fill Upper / Lower	Fill Volume (ft <sup>3</sup> )	Flow Rate (ft <sup>3</sup> /Sec)	Time Before		Volume Remaining at Start of Pull Through (ft <sup>3</sup> )	Liquid		Pull Down Distance (in)
			Terminal Pull Through (Sec)			Height (in)		
0/30	1.34	0.130	9.5		0.10	4.4		1.4
0/26.5	1.18	0.130	8.1		0.13	4.8		1.8
0/26.5	1.18	0.092	10.4		0.22	5.7		2.7
0/10	0.45	0.068	4.3		0.16	5.1		2.1
0/6.5	0.29	0.068	2.3		0.18	5.4		2.4

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TABLE II ----- SLOSH OUTFLOW TESTS

Run No.	% Fill Upper/Lower	Flow Rate (ft <sup>3</sup> /Sec)	Dump Valve Open (Sec)	Liquid at Bulkhead (Ref Time)	Flow Valve Open (Sec)	Start of Clear Flow (Sec)	Flow Valve Closed (Sec)	Start of Terminal Pull Thru (Sec)
60	27 - 0	.13	- .32	0	.30	3.34	4.28	----
51	15 - 15	.13	- .32	0	.28	1.86	3.72	----
54	15 - 15	.13	- .32	0	0.02	1.88	1.88	----
41	15 - 15	.092	- .32	0	.14	1.41	2.71	----
42	15 - 15	.092	- .32	0	.78	1.41	3.20	----
50	15 - 15	.092	- .32	0	.25	1.80	2.88	----
59	15 - 15	.092	- .32	0	.25	2.03	3.16	----
44	5 - 5	.068	- .32	0	0.03	1.62	2.55	----
52	5 - 5	.068	- .32	0	.63	1.54	3.17	----
53	5 - 5	.068	- .32	0	.15	2.16	2.58	----
56	5 - 5	.068	- .32	0	.33	1.66	2.73	----
47	3/4 - 3/4	.068	- .32	0	.04	1.71	2.34	----
48	3/4 - 3/4	.068	- .32	0	.88	1.77	----	3.04
49	3/4 - 3/4	.068	- .32	0	.28	1.73	----	2.30
56	3/4 - 3/4	.068	- .32	0	-0.16	1.79	2.07	----
57	3/4 - 3/4	.068	- .32	0	0.54	1.52	----	2.54



TEST APPARATUS

Figure 1

D

C

B

A

5

1

4

1 BALL BEARING (3)

WELD

2812-1 BRACE (3)  
EQUALLY SPACED  
AROUND GUIDE ASSY

AN3-5A BOLT (2)  
AN1903-10L WASHER (4)  
AN315-5E NUT (2)  
TYP 3 PLACES

28130-1 BLADE -

AN135-3A NUT (32)  
AN1900-10L WASHER (32)

MATCH DRILL AND  
TAP 5/16-18 UNF-3B  
AN6-12A BOLT (2) THREADED  
TO WITHIN .10 OF THE HEAD  
AN560-616 WASHER (2)  
SECTION A-A  
28129-1 GASKET -  
2.500 HOLE - LOCATE TO  
INSTRUCTION BY DEPT 562-1

445 TYP

28128-1 OUTLET ASSY

5

9

1

4

EB118-1 COLLAR (2)

- 2B/20-1 SPRING

- 28/15-1 COLLAB

2017-1 COLLAP

1.375 HOLE DN R WITH 1.630

2B46-1 GUNGE ASSY

DDME SECTION 6

AN6227519 PACKING

-2511-. TUBE ASSY

5 RUBBER GASKET

- 1312 H248

7524254210 44624

AN6295216 P1078

ANDERSON FURNACE WASHER

—2B106-1 RING 2.35

→ EB107-1 GASKET

- PC105-1 CENTER SECTION

415210

**DUMP VALVE**

—20113-1 GATE ASS

...2030-1 SECRET

- ANG-64 BOLT 30,  
A100-64 ANG-64 60  
A100-64 BOLT 30

THANK LETTERS

ITEMS INDICATED \* SUPPLIED  
BY DEPT 562-1  
NOTE:

**NOTE:**

- 1968 SALE - DATE TO  
INSTRUCTION BY DEPT 562-1

- 20122-1 OUTLET

20123-9 CA-657

— 2012:1 COVER

22-104 10.7.6  
 -AI 365-7 - WASHER 3  
 22-104 10.7.6

- At 5:00 PM, WASHDC

AK 215-521, 520

REQUIREMENTS PER ASS

DATE	ONE RECORD NO	SERIAL NO	WEST ASSY
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DESK NO.	CMS RECORD NO.	SERIAL NO.	WEST ASSY.
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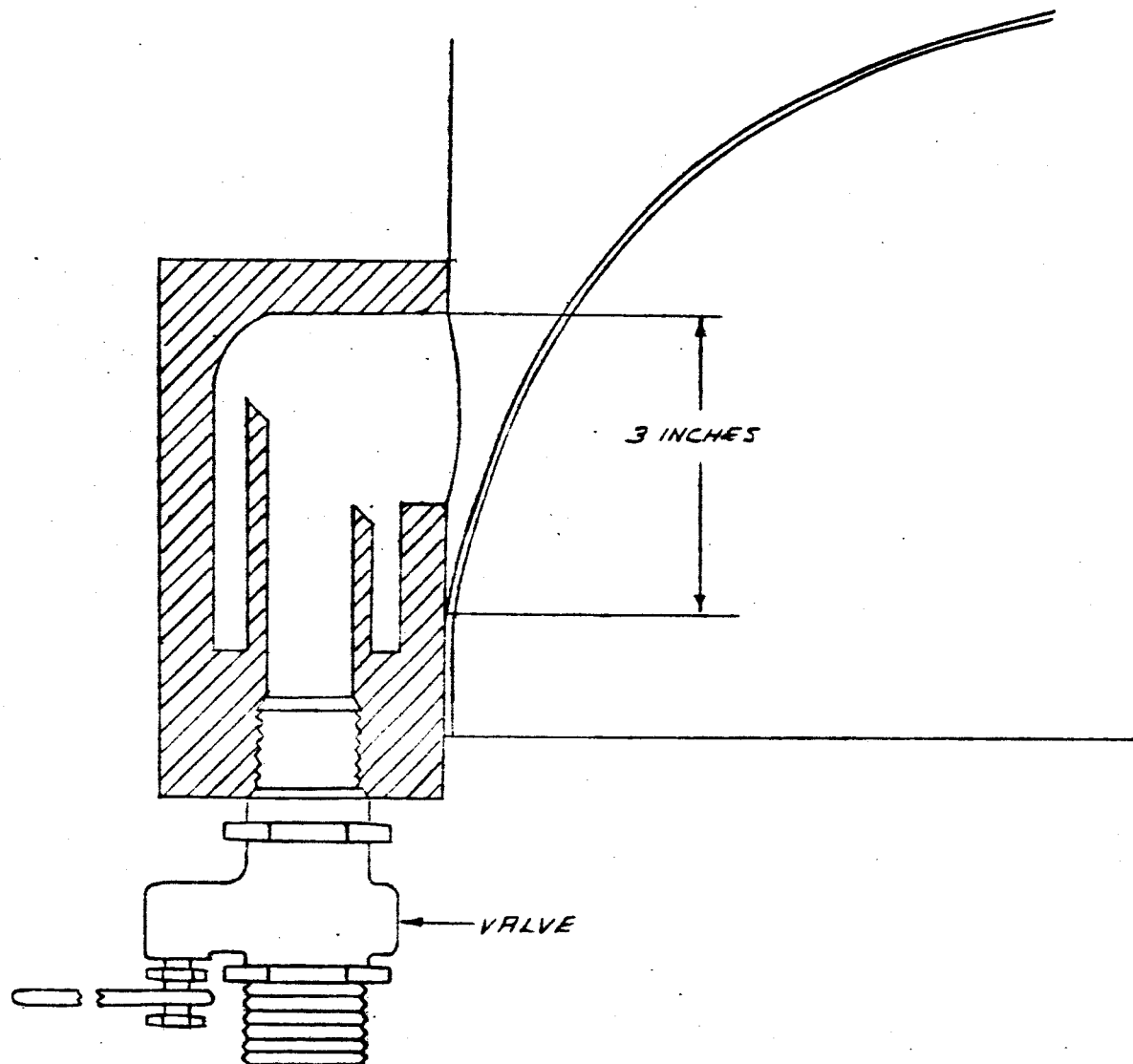
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2



OUTLET ELBOW

FIGURE 3

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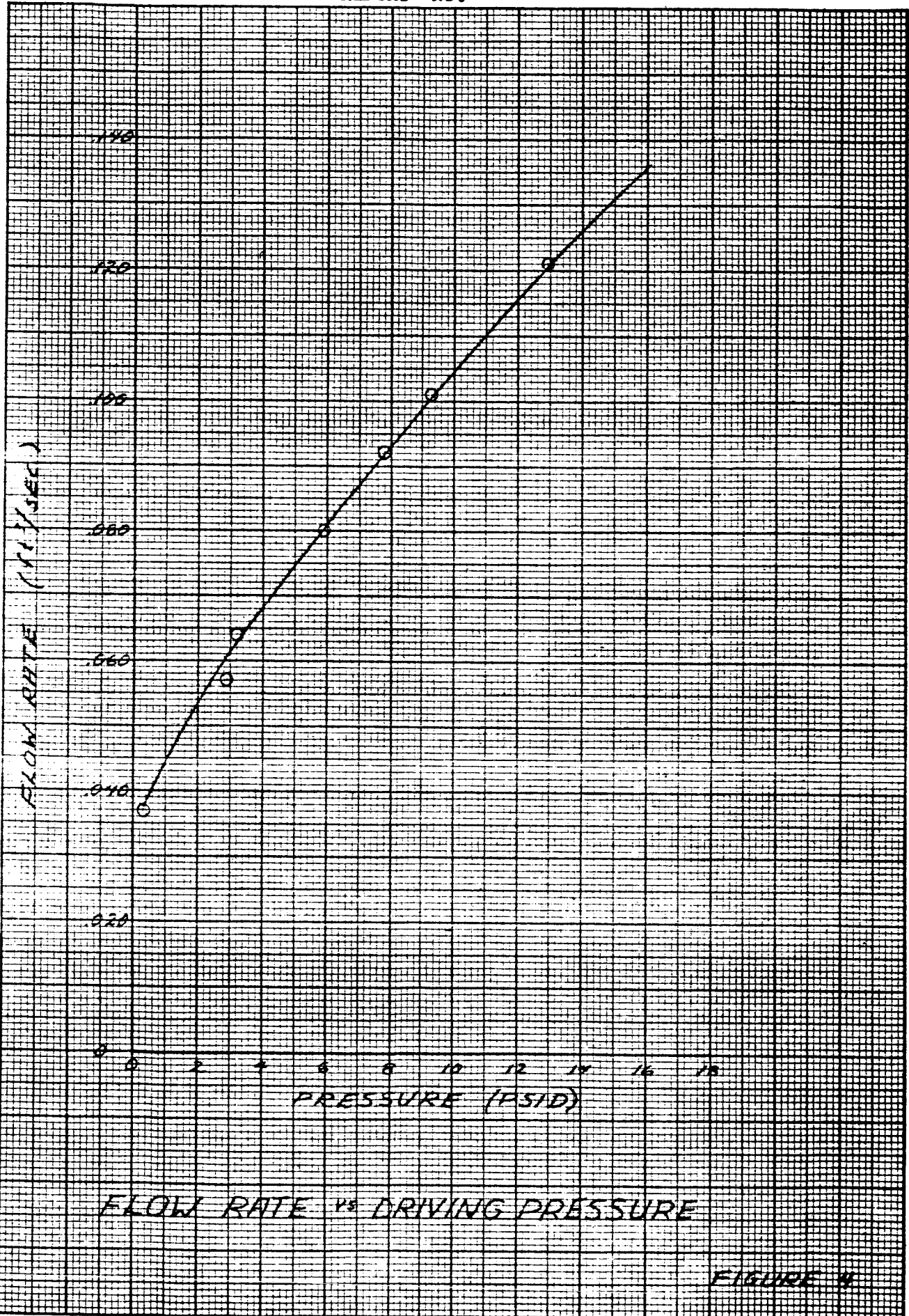
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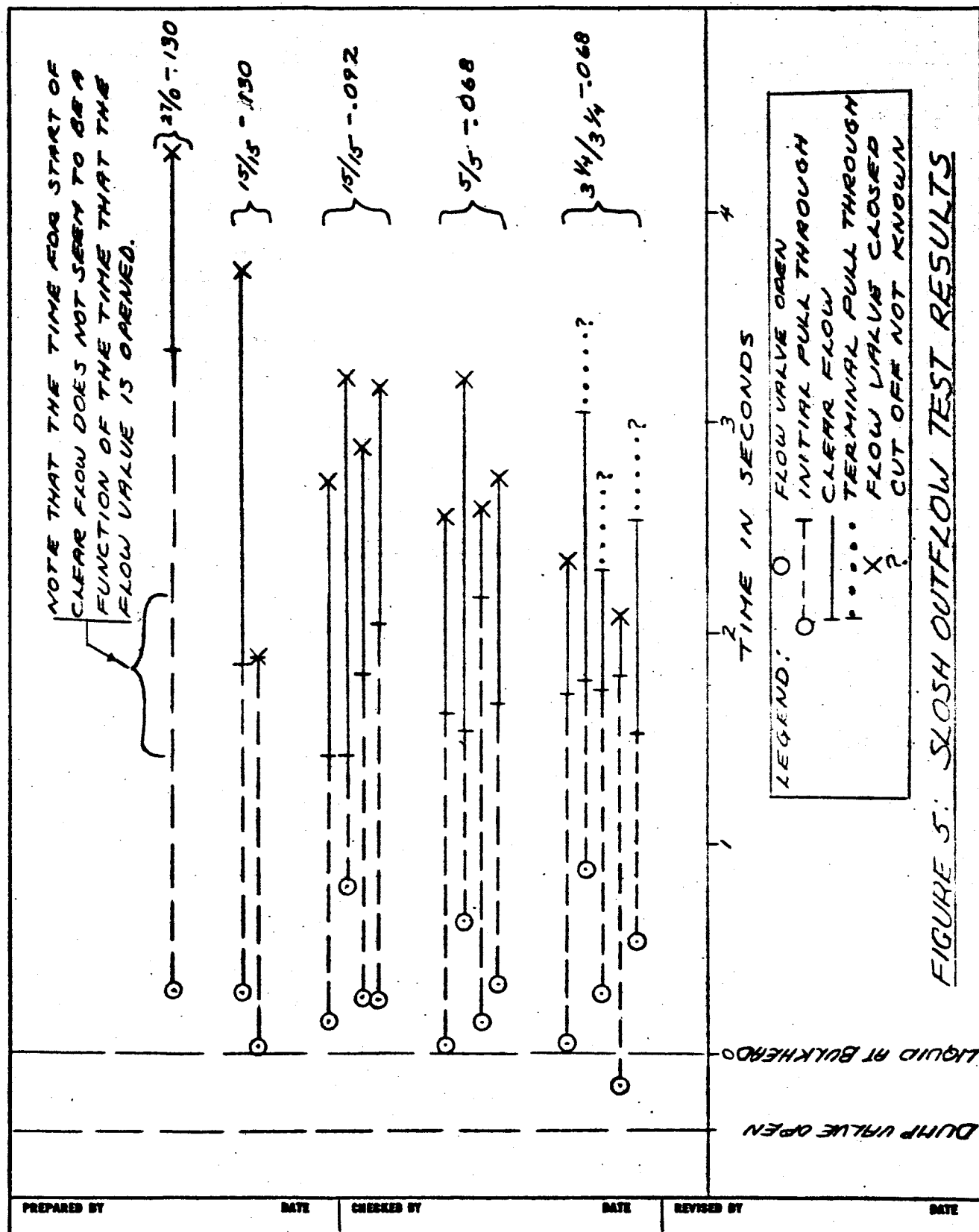
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